



# Sustainable Jet Fuel from Flexible Waste Biomass



## EU Horizon2020 Project **flexJET**

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EUBCE

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## flexJET project

### Project overview

- Total costs: 15 M Euro
- EU financing: 10 M Euro
- H2020 LCE-20 Programme
- Duration: 48 Months (2018-2022)
- Consortium with 13 partners from 5 EU countries

### Aim

- To build a **pre-commercial demonstration plant** for the production of **SAF** derived from **digested food waste** and **waste vegetable oil** while mapping the full economic social and environmental impact of the technology.



## **EU sustainable aviation vision**

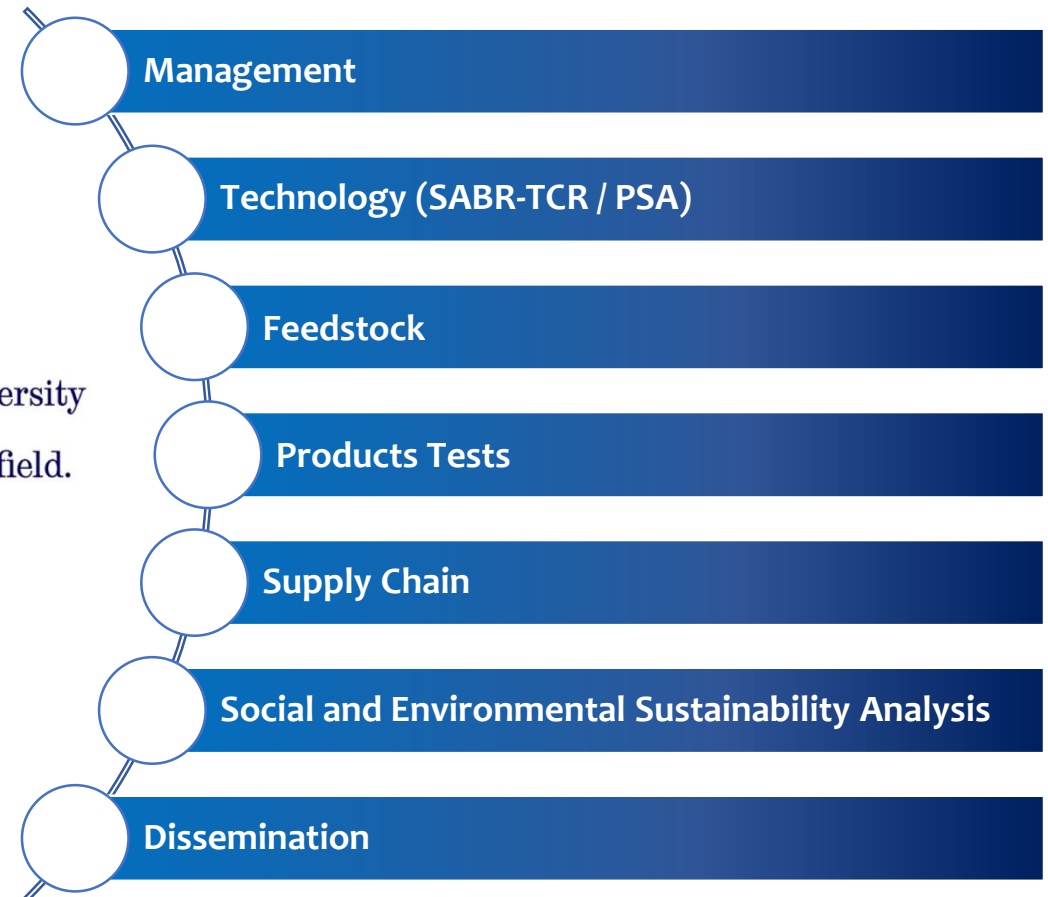
- \* Vision for a climate neutral economy by 2050
- \* Bound Paris agreement to keep global temperature rise to below 1.5 deg C
- \* RED amended in 2015 to include a voluntary opt in for aviation taken up by UK
- \* EU has invested approx. Euro 5 Billion over last 10 Years to support these commitments
- \* In 2016 aviation accounted for 3.6% of all EU28 GHG emissions (13.4% from transport sector)
- \* Aviation emissions more than doubled since 1990 (will continue to become more significant as other sectors decarbonise)



## Partners



The University Of Sheffield.





- From feedstock diversification assessment

- Through environmental and social sustainability evaluation of the process

- To commercial uptake facilitation of cost-competitive aviation fuel

By contributing to the Renewable Energy Directive targets for renewable energy and to the fulfillment of the CORSIA targets

**Kick –off**  
April 2018

**Plant Design**  
Mid 2019

**Demo Plant**  
Mid 2020

**SAF Delivery**  
End 2021

**End of Project**  
Mid 2022





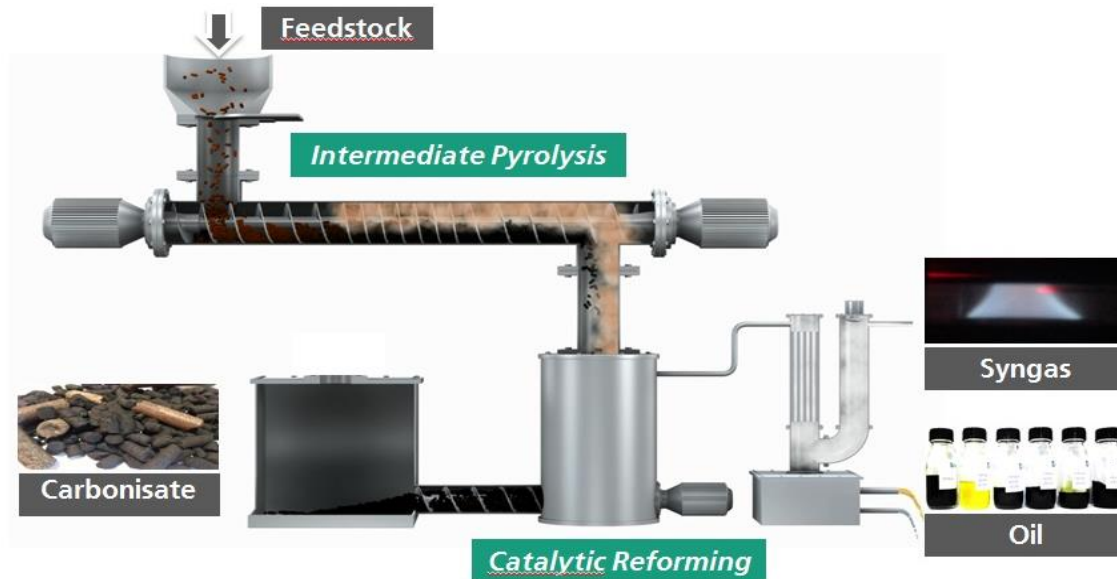
## Objectives

- Demonstrate the technical viability of aviation fuel production from waste biomass compliant under ASTM D7566
- Evaluate the environmental and social sustainability of the process
- Contribute to the Renewable Energy Directive targets for renewable energy
- Facilitate towards commercial uptake of the technology



## Combination of Two Innovative Technologies

### TCR® (Thermo-Catalytic Reforming)



### SABR (Transesterification)



Source:





- TCR (Thermo-Catalytic Reforming)
- 500 Kg/h Biomass Plant

- TCR (Thermo-Catalytic Reforming)
- 30 Kg/h Biomass Plant







## TCR Feedstock





### TCR Crude Products

#### BIO-OIL



C	76.6 wt.%
H	7.7 wt.%
N	2.2 wt.%
S	0.6 wt.%
O (diff.)	11.2 wt.%
H <sub>2</sub> O	1.7 wt.%
Ash	< 0.05 wt.%
TAN	4.9 mg KOH/g
HHV	33.9 MJ/kg

- miscible with fossil/bio fuels
- low tar content and acidity
- low fraction of non-volatiles

#### SYNGAS



H <sub>2</sub>	35 ± 3 v/v%
CO	15 ± 2 v/v%
CO <sub>2</sub>	25 ± 1 v/v%
CH <sub>4</sub>	7 ± 2 v/v%
C <sub>x</sub> H <sub>y</sub>	2 ± 1 v/v%
N <sub>2</sub> (diff.)	16 ± 2 v/v%
HHV	11 MJ/m <sup>3</sup>

- tar and dust free gas
- H<sub>2</sub> over 30 v/v%

#### CHAR



C	65.0 wt.%
H	1.2 wt.%
N	1.5 wt.%
S	0.3 wt.%
O (diff.)	2.2 wt.%
H <sub>2</sub> O	0.7 wt.%
Ash	29.1 wt.%
HHV	23.9 MJ/kg

- high mechanical stability
- transportable and storable
- low-odour



## TCR Oil After Upgrading

### TCR® BIO-OIL



C	77.6 wt.%
H	8.0 wt.%
N	4.6 wt.%
S	0.6 wt.%
O (diff.)	7.0 wt.%
H <sub>2</sub> O	2.2 wt.%
Ash	< 0.005 wt.%

LHV	34.0 MJ/kg
TAN	2.1 mg KOH/g
Viscosity	4,428 mm <sup>2</sup> /s
Density	1014.4 kg/m <sup>3</sup>

- miscible with fossil/bio fuels
- low tar content and acidity
- low fraction of non-volatiles

### TCR® BIO-OIL, HDO



C	86.2 wt.%
H	13.0 wt.%
N	< 0.5 wt.%
S	0.01 wt.%
O (diff.)	< 0.7 wt.%
H <sub>2</sub> O	0.003 wt.%
Ash	< 0.005 wt.%

LHV	42.25 MJ/kg
TAN	0.0 mg KOH/g
Viscosity	0,97 mm <sup>2</sup> /s
Density	815.7 kg/m <sup>3</sup>

- Outstanding fuel quality





- SABR Plant Green Fuels
- Transesterification (50,000 Litres Per Day FAME Production)





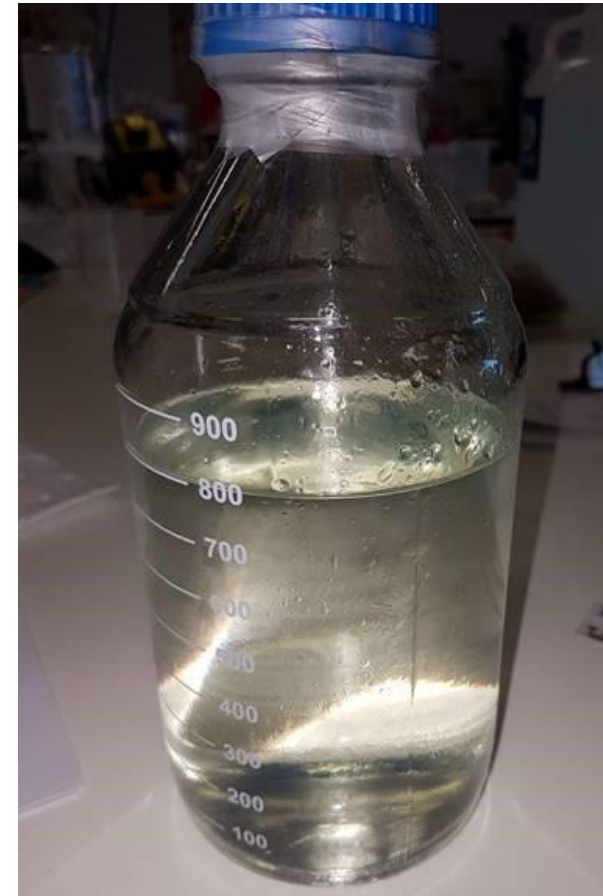
## HEFA Production

### \* Optimisation:

- \* HDO reaction temperature
- \* HC reaction temperature
- \* H<sub>2</sub> pressure

### Fractional distillation results:

- Up to 55 vol.% at Jet Fuel fraction
- 45 vol.% Others  
(including green diesel and gasoline)

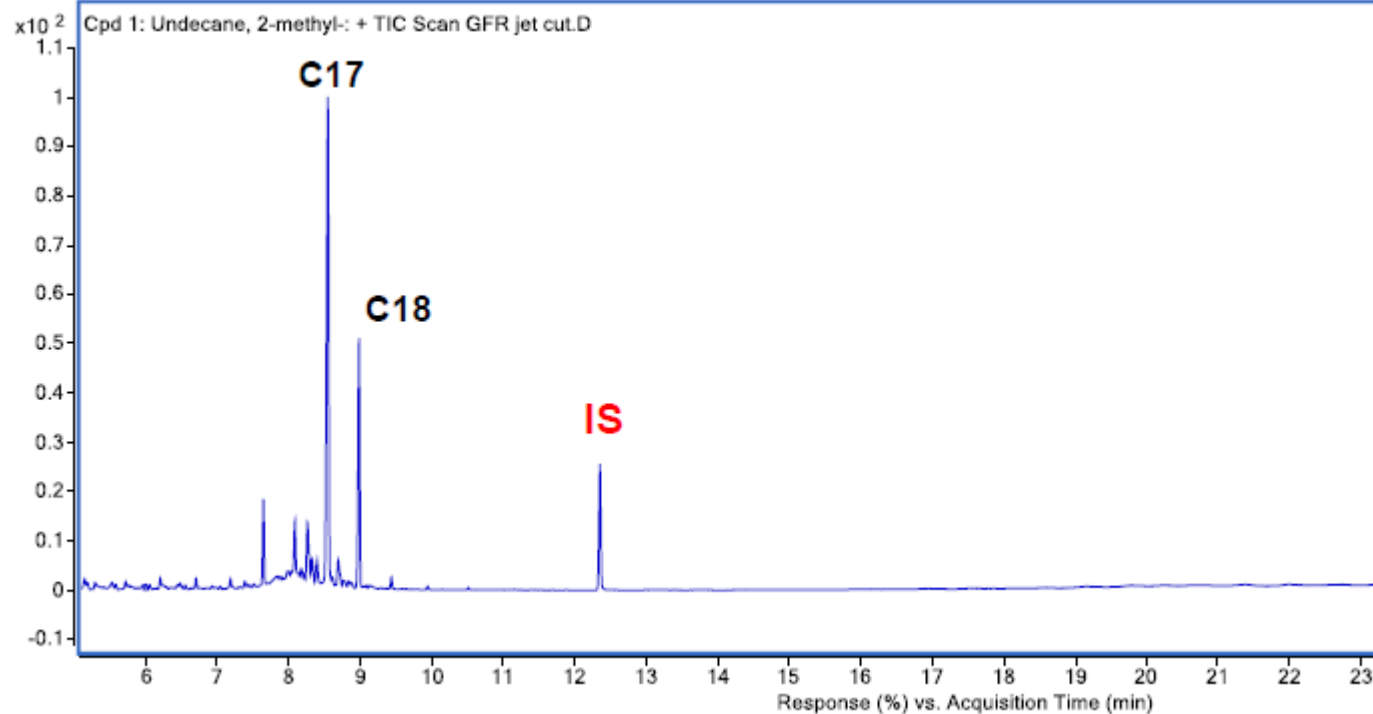


Sample after HDO + HC



## Results

### HEFA Production – GC-MS Jet Fuel Cut



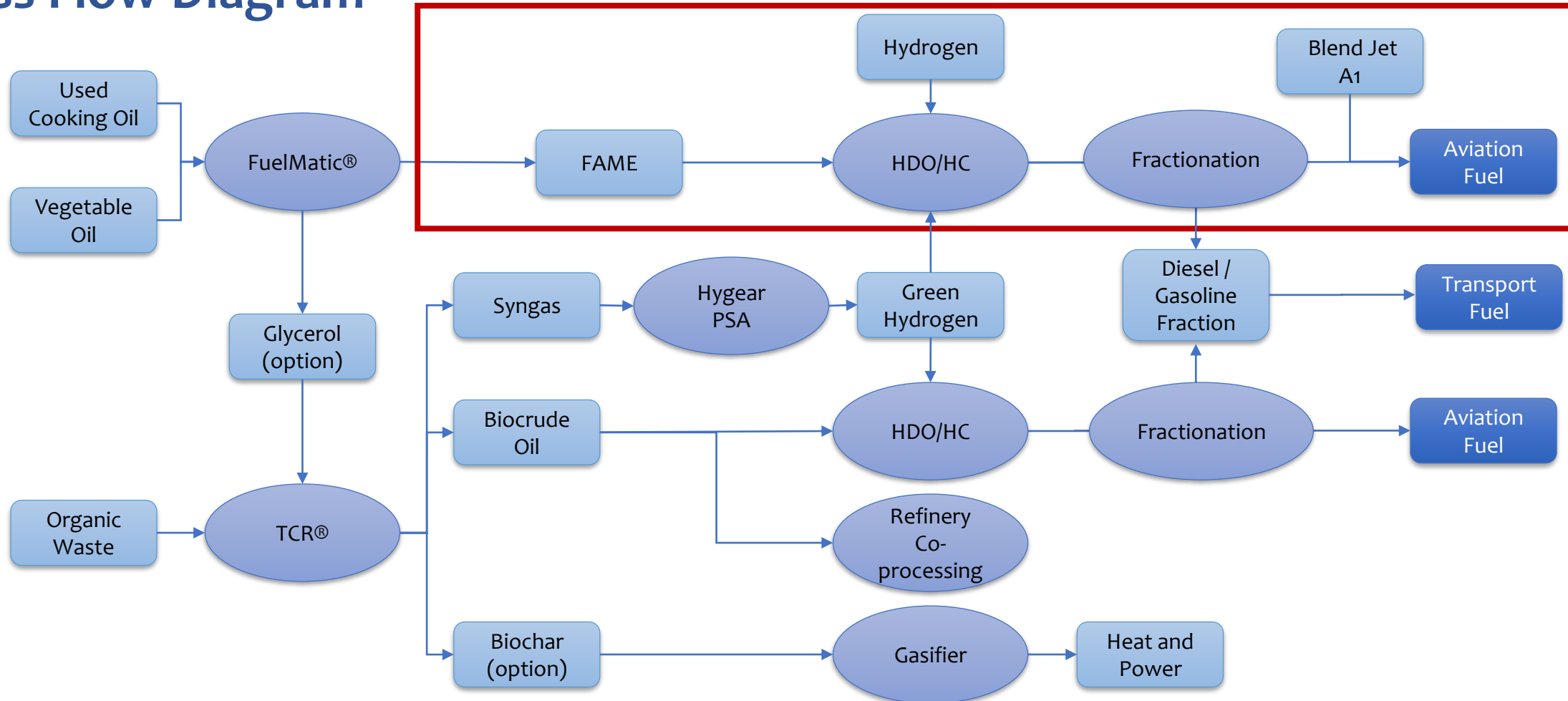
CAS	Name	Mass (DB)	Formula (C Area	RT
7045-71-8	Undecane, 2-methyl-	170.2	C12H26	273375 6
1002-43-3	Undecane, 3-methyl-	170.2	C12H26	177898 6.054
08/02/3913	1-Octanol, 2-butyl-	186.2	C12H26O	685417 6.2
08/02/3913	1-Octanol, 2-butyl-	186.2	C12H26O	58053 6.33
2425-77-6	1-Decanol, 2-hexyl-	242.3	C16H34O	130120 6.378
1000382-54-3	Carbonic acid, eicosyl vinyl ester	368.3	C23H44O3	206785 6.443
1000382-54-3	Carbonic acid, eicosyl vinyl ester	368.3	C23H44O3	150025 6.551
629-50-5	Tridecane	184.2	C13H28	348101 6.702
1000382-54-3	Carbonic acid, eicosyl vinyl ester	368.3	C23H44O3	129790 6.972
14905-56-7	Tetradecane, 2,6,10-trimethyl-	240.3	C17H36	613082 7.183
638-36-8	Hexadecane, 2,6,10,14-tetramethyl-	282.3	C20H42	399877 7.383
629-62-9	Pentadecane	212.3	C15H32	2826201 7.642
638-36-8	Hexadecane, 2,6,10,14-tetramethyl-	282.3	C20H42	374519 7.713
638-36-8	Hexadecane, 2,6,10,14-tetramethyl-	282.3	C20H42	2407773 7.848
629-94-7	Heneicosane	296.3	C21H44	1778818 7.993
629-94-7	Heneicosane	296.3	C21H44	4223213 8.085
13475-75-7	Pentadecane, 8-hexyl-	296.3	C21H44	1020666 8.172
13475-75-7	Pentadecane, 8-hexyl-	296.3	C21H44	537466 8.215
629-94-7	Heneicosane	296.3	C21H44	3256478 8.258
13475-75-7	Pentadecane, 8-hexyl-	296.3	C21H44	1455590 8.323
1560-89-0	Heptadecane, 2-methyl-	254.3	C18H38	1506823 8.393
629-78-7	Heptadecane	240.3	C17H36	20811011 8.544
45235-48-1	1-Decanol, 2-octyl-	270.3	C18H38O	518202 8.609
110225-00-8	1-Dodecanol, 2-hexyl-	270.3	C18H38O	1675503 8.69
110225-00-8	1-Dodecanol, 2-hexyl-	270.3	C18H38O	587325 8.766
04/11/2665	Trihexadecyl borate	734.8	C48H99BC	441472 8.836
593-45-3	Octadecane	254.3	C18H38	8499693 8.982
629-92-5	Nonadecane	268.3	C19H40	438586 9.436
1731-92-6	Heptadecanoic acid, methyl ester	284.3	C18H36O2	4455813 12.353





## Process Flow Diagram

**HEFA – ASTM D7566**









## Prince Charles Site Visit

- Invitation to open plant
- Invitation to BBC for dissemination
- First UK plant delivering SAF







## flexJET Advantages

- \* High feedstock flexibility
- \* Green Hydrogen
  - \* Hydrogen separated from TCR<sup>®</sup> Syngas by PSA to be used in HDO / HC
- \* Side and end products flexibility
- \* Highly scalable (small scale decentralised facilities can be built)
- \* It can be integrated into existing infrastructure

# CONSORTIUM

Coordinator



UNIVERSITY OF  
BIRMINGHAM

Partners



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Duration  
April 2018 - March 2022

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